

**Amendments to the Claims:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

1. (Canceled)
2. (Previously presented) The process according to claim 24, wherein the oxygenates and unsaturates are selected from the group consisting of normal alcohols, mono-olefins, and mixtures thereof.
3. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least 0.5 wt% normal alcohols as oxygenates.
4. (Original) The process of claim 3, wherein the normal alcohols boil in the range of from about 50°C to about 350°C.
5. (Canceled)
6. (Canceled)
7. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 5.0 wt % mono-olefins.
8. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 15.0 wt % mono-olefins.
9. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 25.0 wt % mono-olefins.
10. (Original) The process of claim 9, wherein the mono-olefins boil in the range of from about -105 to 350°C.

11. (Previously presented) The process of claim 24, wherein the Fischer-Tropsch hydrocarbon stream is a low-boiling fraction in a range from about -65°C to about 350°C.
12. (Canceled)
13. (Canceled)
14. (Canceled)
15. (Canceled)
16. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is from a hydrogen production unit.
17. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is recycled from a hydroprocessing operation.
18. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is syngas.
19. (Canceled)
20. (Canceled)
21. (Canceled)
22. (Canceled)
23. (Canceled)

24. (Currently amended) A process for hydroconversion of a Fischer-Tropsch hydrocarbon stream including oxygenates and hydrocarbon unsaturates with reduction in formation of heavy molecular weight products during heating, the process comprising:
- a) adding a first hydrogen-containing gas to the hydrocarbon stream not under hydroconversion conditions, wherein the first hydrogen-containing gas is sufficient to reduce the amount of heavy molecular weight products formed during heating as compared to a heated hydrocarbon stream without added hydrogen, to form a mixed stream;
  - b) heating the mixed stream;
  - c) adding a second hydrogen-containing gas to the heated mixed stream sufficient to effect hydroconversion of the mixed stream, to form a hydroconversion feed stream;
  - d) heating the hydroconversion feed stream to reaction temperature; and
  - e) hydroconverting the hydroconversion feed stream.
25. (Original) The process of claim 24, wherein the first hydrogen-containing gas is added in an amount less than about 500 Standard Cubic Feet per Barrel (SCFB).
26. (Original) The process of claim 25, wherein the first hydrogen-containing gas is added in an amount less than about 100 SCFB.
27. (Original) The process of claim 26, wherein the first hydrogen-containing gas is added in an amount less than about 50 SCFB.
28. (Original) The process of claim 24, wherein the second hydrogen-containing gas is added in an amount less than 750 SCFB.
29. (Previously presented) The process of claim 24, wherein the mixed stream is heated to a temperature in the range of from about 120°C to about 400°C.

30. (Original) The process of claim 24, wherein the mixed stream is heated to a temperature in the range of from about 250°C to about 400°C.